

LISTING OF CLAIMS

1-9. (canceled)

10. (currently amended) **An oriented web produced from A polypropylene web comprising a perforated extruded sheet comprising a propylene polymer comprising beta-spherulites in an amount sufficient to produce a K-value of about 0.2 to 0.95 when measured by x-ray diffraction or to show a beta crystalline melting peak during the first or second heating scan when measured using a differential scanning calorimeter, wherein the oriented web is biaxially oriented and wherein the web has thickness in the node junction region between the machine direction and transverse direction strands that is at least 10% less than that of a biaxially oriented web made from an extruded polypropylene sheet with no added beta nucleant and the same starting sheet thickness.**

11. (withdrawn – currently amended) A method for making an oriented **polypropylene** web, wherein the oriented web is uniaxially oriented or biaxially oriented and wherein the web has thickness in the node junction region between the machine direction and transverse direction strands that is at least 10% less than that of a **uniaxially oriented or** biaxially oriented web made from an extruded **polypropylene** sheet with no added beta nucleant and the same starting sheet thickness, the method comprising the steps of:

(a) feeding a concentrate and a resinous **[[poly]]**propylene polymer to an extruder to melt from a polymeric sheet, wherein the concentrate comprises a **[[poly]]**propylene resin and a beta-nucleating agent, wherein the beta-nucleating agent is present in a concentration in a range of 1.2% to 0.036% by weight of the total polymer content **or between 12,00 and 360 ppm,**

(b) quenching the polymeric sheet at a quench temperature sufficient to produce a **[[poly]]**propylene sheet comprising beta-spherulites in an amount sufficient to produce a K-value of about 0.2 to 0.95 when measured by x-ray diffraction or to show a beta crystalline

melting peak during the first or second heating scan when measured using a differential scanning calorimeter,

(c) extruding the quenched sheet,

(d) perforating the extruded sheet, and

(e) orienting the perforated sheet uniaxially or biaxially, wherein the orienting step comprises heating the perforated sheet to a temperature less than or equal to 155 °C.

12. (canceled)

13. (currently amended) The oriented web of claim **[[12]] 10**, wherein the extruded sheet can be run at line speeds that are at least 5% faster than the line speeds for an extruded polypropylene sheet with no added beta nucleant and the same starting thickness.

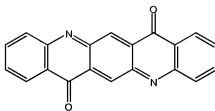
14. (currently amended) The oriented web of claim **[[12]] 10**, wherein the oriented web has a tensile strength measured at 2% elongation in the machine direction, that is at least 10% higher than that of a biaxially oriented web made from an extruded polypropylene sheet with no added beta nucleant and the same starting thickness.

15. (currently amended) The oriented web of claim **[[12]] 10**, wherein the oriented web has a tensile strength measured at 5% elongation in the machine direction, that is at least 10% higher than that of a biaxially oriented web made from an extruded polypropylene sheet with no added beta nucleant and the same starting thickness.

16. (currently amended) The oriented web of claim **[[12]] 10**, wherein the oriented web has a torsional rigidity that is at least 10% higher than that of a biaxially oriented web made from an extruded polypropylene sheet with no added beta nucleant and the same starting thickness.

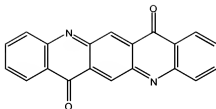
17. (withdrawn) A concentrate comprising a polypropylene resin and a beta-nucleating agent, wherein the beta-nucleating agent is present in a concentration in a range of 1.2% to 0.036% by weight of the total polymer content ~~or between 12,000 and 360 ppm~~.

18. (withdrawn) The concentrate of claim 17, wherein the beta-nucleating agent is present in a concentration of 0.047% by weight of the total polymer content ~~or 470 ppm~~.
19. (withdrawn) The concentrate of claim 17 wherein the polypropylene is selected from the group consisting of polypropylene homopolymer and copolymers of polypropylene containing other alpha-olefin monomers.
20. (withdrawn) The concentrate of claim 17 in the form of a pellet.
21. (withdrawn – previously presented) The concentrate of claim 17 wherein the beta-nucleating agent has the structural formula:

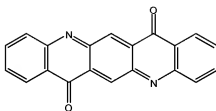


22. (withdrawn) The concentrate of claim 17 further comprising an additive selected from the group consisting of lubricants, antioxidants, ultraviolet absorbers, radiation resistant agents, antiblocking agents, antistatic agents, coloring agents, and opacifiers, which do not nucleate the alpha crystal form of polypropylene.
23. (withdrawn) The method of claim 11, wherein step (a) further comprises feeding to the extruder an additive selected from the group consisting of lubricants, antioxidants, ultraviolet absorbers, radiation resistant agents, antiblocking agents, antistatic agents, coloring agents, and opacifiers, which do not nucleate the alpha crystal form of polypropylene.
24. (withdrawn and previously presented) The method of claim 11, wherein step (c) comprises stretching the perforated sheet at a higher drawing rate relative to a drawing rate used to stretch a perforated polypropylene sheet with no added beta nucleant and the same starting thickness.

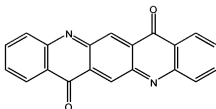
25. (currently amended) An oriented web produced from ~~the polypropylene web of claim 10 a~~ **perforated extruded sheet comprising a propylene polymer comprising beta-spherulites in an amount sufficient to produce a K-value of about 0.2 to 0.95 when measured by x-ray diffraction or to show a beta crystalline melting peak during the first or second heating scan when measured using a differential scanning calorimeter,** wherein the oriented web is uniaxially oriented and wherein the web has thickness in the node junction region between the machine direction and transverse direction strands that is at least 10% less than that of a uniaxially oriented web made from an extruded sheet with no added beta nucleant and the same starting sheet thickness.
26. (previously presented) The oriented web of claim 25, wherein the extruded sheet can be run at line speeds that are at least 5% faster than the line speeds for an extruded polypropylene sheet with no added beta nucleant and the same starting thickness.
27. (previously presented) The oriented web of claim 25, wherein the oriented web has a tensile strength measured at 2% elongation in the machine direction, that is at least 10% higher than that of a uniaxially oriented web made from an extruded polypropylene sheet with no added beta nucleant and the same starting thickness.
28. (previously presented) The oriented web of claim 25, wherein the oriented web has a tensile strength measured at 5% elongation in the machine direction, that is at least 10% higher than that of a uniaxially oriented web made from an extruded polypropylene sheet with no added beta nucleant and the same starting thickness.
29. (previously presented) The oriented web of claim 25, wherein the oriented web has a torsional rigidity that is at least 10% higher than that of a uniaxially oriented web made from an extruded polypropylene sheet with no added beta nucleant and the same starting thickness.
30. (new) The oriented web of claim 25, wherein the beta-spherulites are produced by addition of a beta-nucleating agent having the structural formula:



31. (new) The oriented web of claim 25, wherein the propylene polymer is selected from polypropylene homopolymer and copolymers of polypropylene containing other alpha-olefin monomers.
32. (new) The oriented web of claim 10, wherein the beta-spherulites are produced by addition of a beta-nucleating agent having the structural formula:



33. (new) The oriented web of claim 10, wherein the propylene polymer is selected from polypropylene homopolymer and copolymers of polypropylene containing other alpha-olefin monomers.
34. (withdrawn – new) The method of claim 11, wherein the beta-nucleating agent has the structural formula:



35. (withdrawn – new) The method of claim 11, wherein the propylene polymer is selected from polypropylene homopolymer and copolymers of polypropylene containing other alpha-olefin monomers.
36. (withdrawn – new) The method of claim 11, wherein the extruded sheet is run at line speeds that are at least 5% faster than the line speeds for an extruded polypropylene sheet with no added beta nucleant and the same starting thickness.